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# Elimination behavior of nitrog[en](http://www.elsevier.com/locate/tca) [oxides](http://www.elsevier.com/locate/tca) [from](http://www.elsevier.com/locate/tca) [a](http://www.elsevier.com/locate/tca) NO $_3^{\texttt{-}}$ -intercalated Mg–Al layered double hydroxide during thermal decomposition

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## **1. Introduction**

## ABSTRACT

The thermal properties of NO<sub>3</sub><sup>-</sup>-intercalated Mg–Al layered double hydroxide (NO<sub>3</sub>·Mg–Al LDH) were investigated using simultaneous thermogravimetry–mass spectrometry (TG–MS), and the elimination behavior of nitrogen oxides from this double hydroxide was examined. The TG–MS results showed that NO3·Mg–Al LDH decomposed in four stages. The first stage involved evaporation of surface adsorbed water and interlayer water in  $NO_3 \cdot Mg-A$ l LDH. In the second and third stages, dehydroxylation of the brucite-like octahedral layers in NO3·Mg–Al LDH occurred. The fourth stage mainly corresponded to the elimination of NO3 $^{\rm -}$  intercalated in the Mg–Al LDH interlayers to afford NO $_{\rm 2}$ . Thermal decomposition of NO<sub>3</sub>·Mg–Al LDH at 400–600 °C resulted in the formation of Mg–Al oxide, and the produced NO<sub>2</sub> reacted with H<sub>2</sub>O and  $O_2$  to form HNO<sub>3</sub> and HNO<sub>2</sub>. The elimination of nitrogen oxides was found to increase with time and decomposition temperature. The synthesized Mg–Al oxide mixture could be used to remove nitric acid from aqueous solutions.

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It has been found that Mg–Al layered double hydroxide (Mg–Al LDH) can be used as an adsorbent for the removal of anionic pollutants in aqueous media [1–8]. Mg–Al LDH can be used as an anion exchanger [9] and is represented by the formula  $[Mg^{2+}{}_{1-x}Al^{3+}{}_{x}(OH)_2](A^{n-})_{x/n}$ · $mH_2O$ , where  $A^{n-}$  is an anion such as CO3 $^{2-}$  and Cl<sup>−</sup>, and x is the Al/(Mg + Al) molar ratio (0.20  $\le$  x  $\le$  0.33) [10,11]. Mg–Al LDH consists of brucite-like octahedral layers that are positively charg[ed](#page-4-0) [beca](#page-4-0)use of the replacement of some  $Mg^{2+}$ units by  $Al^{3+}$ , [while](#page-4-0) the interlayer anions help in maintaining charge balance. Water  $(H<sub>2</sub>O)$  molecules occupy the remaining spaces in the interlayer.  $CO_3^2$ <sup>-</sup>-intercalated Mg–Al LDH ( $CO_3$ ·Mg–Al LDH) can be converted to Mg–Al oxide by calcination at 450–800 ◦C. The formation of Mg–Al oxide is represented by the following reaction:

$$
Mg_{1-x}Al_x(OH)_2(CO_3)_{x/2} \to Mg_{1-x}Al_xO_{1+x/2} + (x/2)CO_2 + H_2O \quad (1)
$$

The resulting Mg–Al oxide undergoes rehydration and combines with anions to afford the original LDH structure, as shown in the following equation:

$$
Mg_{1-x}Al_xO_{1+x/2}+x/nA^{n-}+(1+x/2)H_2O\\
$$

 $\rightarrow$  Mg<sub>1-x</sub>Al<sub>x</sub>(OH)<sub>2</sub>A<sub>x/n</sub> + xOH<sup>-</sup> (2)

The abovementioned rehydration and subsequent combination of Mg–Al oxide with anions in solution are accompanied by the release of OH−. Accordingly, Mg–Al oxide can neutralize and fix  $NO_{3}^-$  when used in the treatment of HNO $_{3}$  [12]. Subsequently,  $NO<sub>3</sub>$ –-intercalated Mg–Al LDH ( $NO<sub>3</sub>$ -Mg–Al LDH) is produced by the reconstruction of Mg–Al oxide. In actual wastewater treatment, large quantities of Mg–Al oxide are used, and hence, considerable amounts of waste  $NO<sub>3</sub>$ ·Mg-Al LDH are generated. If Mg-Al oxide can be regenerat[ed](#page-4-0) from the obtained  $NO<sub>3</sub>$  $NO<sub>3</sub>$ ·Mg-Al LDH and reused to treat waste  $HNO<sub>3</sub>$ , the energy required for the synthesis of Mg-Al oxide and  $CO<sub>3</sub>$ ·Mg-Al LDH will be drastically reduced, and the formation of NO<sub>3</sub>·Mg-Al LDH wastes can be prevented. In order to effectively reuse Mg–Al oxide for the treatment of  $HNO<sub>3</sub>$ , it is necessary to examine in detail the thermal decomposition behavior of  $NO<sub>3</sub>$  Mg–Al LDH and the elimination of nitrogen oxides.

In this study, we investigated the thermal properties of NO3·Mg–Al LDH by simultaneous thermogravimetry–mass spectrometry (TG–MS). In addition, we carried out thermal decomposition of NO<sub>3</sub>·Mg-Al LDH in air and investigated the effect of temperature on its elimination behavior of nitrogen oxides. We also examined the capability for the treatment of  $HNO<sub>3</sub>$  with Mg-Al oxides obtained by the thermal decomposition of NO<sub>3</sub>·Mg-Al LDHs at different temperature.

## **2. Experimental**

## 2.1. Preparation

NO3·Mg–Al LDH was prepared by the co-precipitation method. The Mg–Al solution  $(0.4 M Mg(NO<sub>3</sub>)<sub>2</sub> + 0.1 M Al(NO<sub>3</sub>)<sub>3</sub>)$  was pre-

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Fig. 1. Experimental apparatus used for thermal decomposition of NO<sub>3</sub> Mg-Al LDH. (1) Air cylinder; (2) flow meter; (3) thermocouple; (4) sample; (5) electric furnace; (6) quartz reaction tube; (7) aluminum boat; (8) flexible heater; and (9) water trap  $(0^{\circ}C).$ 

pared by dissolving  $Mg(NO_3)_2.6H_2O$  (0.1 mol) and  $Al(NO_3)_3.9H_2O$ (0.025 mol) in 250 mL of deionized water. The Mg–Al solution was added dropwise to 250 mL of 0.3 mM NaOH solution at 30 ◦C with mild agitation. The solution pH was adjusted to 10.5 by adding 0.5 M NaOH solution. The mixture was then stirred continuously at 30 ◦C for 1 h. The  $NO<sub>3</sub>·Mg-Al$  LDH that formed was isolated by filtering the resulting suspension, washing it thoroughly with deionized water, and drying it under reduced pressure (133 Pa) at  $40^{\circ}$ C for 40 h. The  $NO<sub>3</sub>$ ·Mg–Al LDH crystals were ground into powder using a mortar and pestle, and the resulting powder was characterized by X-ray diffraction (XRD) using a Rigaku RINT-2200VHF diffractometer (Rigaku Corp., Tokyo, Japan) with CuK $\alpha$  radiation at 40 kV and 20 mA (scan rate:  $2°$  min<sup>-1</sup>). The NO<sub>3</sub> Mg-Al LDH was dissolved in 1 M HNO<sub>3</sub>, and analyzed for Mg<sup>2+</sup> and Al<sup>3+</sup> using inductively coupled plasma–atomic emission spectrometry (ICP–AES). The  $NO<sub>3</sub>·Mg-Al$  LDH was also dissolved in 0.1 M HCl, and analyzed for NO $_3^-$  using a Dionex DX-120 ion chromatograph equipped with an AS-12A column (eluent: 2.7 mM  $Na<sub>2</sub>CO<sub>3</sub>$  and 0.3 mM NaHCO<sub>3</sub>; flow rate:  $1.3$  mL min<sup>-1</sup>).

## 2.2. Thermal properties of  $NO<sub>3</sub>·Mg-Al$  LDH

A 10-mg sample of  $NO<sub>3</sub>$  Mg-Al LDH was analyzed by simultaneous TG (Seiko Instruments TG/DTA 6200) and MS (Hewlett Packard 5973) at a heating rate of 5 ◦C min−<sup>1</sup> in a He flow rate of 200 mL min−1. The decomposition products were introduced to the MS ion source through an inactivated stainless steel capillary tube heated at 300 ℃ to prevent condensation of the evolved products.

## 2.3. Elimination behavior of nitrogen oxides from  $NO<sub>3</sub>$  Mg-Al LDH

The experimental apparatus used for carrying out the thermal decomposition of NO<sub>3</sub>·Mg-Al LDH is shown in Fig. 1. An aluminum boat containing 0.5 g of NO<sub>3</sub>·Mg-Al LDH was inserted in a quartz reaction tube, which was placed in an electric furnace. NO<sub>3</sub>·Mg-Al LDH decomposed at 400–600 °C at an air flow rate of 50 mL min<sup>-1</sup>. The evolved gas was collected in three water traps  $(0^{\circ}C)$  containing 30 mL deionized water. In order to prevent condensation of the evolved gas, the line from the quartz reaction tube to the trap was heated to 110–130 °C using a flexible heater. The anions in the traps were quantified using ion chromatograph. The products obtained in the thermal decomposition of  $NO<sub>3</sub>$ ·Mg-Al LDH were identified by XRD analysis.

## 2.4. Treatment of HNO<sub>3</sub>

Mg–Al oxides, obtained by the thermal decomposition of  $NO<sub>3</sub>$ ·Mg–Al LDH at 400–600 $°C$  using the experimental apparatus



Fig. 2. XRD patterns for NO<sub>3</sub> Mg-Al LDH.

shown in Fig. 1, were examined to check the capability for the treatment of  $HNO<sub>3</sub>$ . 10 mL of 0.1 M  $HNO<sub>3</sub>$  solution were added to a pre-determined amount of  $Mg_{0.80}Al_{0.20}O_{1.10}$  in 50-mL screw-top tubes, and shaken at 25 °C for 24 h. The quantity of  $Mg_{0.80}Al_{0.20}O_{1.10}$ used was a stoichiometric quantity according to Eq. (3).

$$
Mg_{0.80}Al_{0.20}O_{1.10} + 0.20HNO_3 + 0.90H_2O
$$
  
\n
$$
\rightarrow Mg_{0.80}Al_{0.20}(OH)_2(NO_3)_{0.20}
$$
\n(3)

The NO $_3^-$  concentration of the filtrate was determined using the ion chromatograph.

#### **3. Results and discussion**

#### 3.1. Preparation

The XRD patterns obtained for  $NO<sub>3</sub> \cdot Mg-Al$  LDH (Fig. 2) are ascribed to hydrotalcite (JCPDS card 22-700), a naturally occurring hydroxycarbonate of magnesium and aluminum  $(Mg_6Al_2(OH)_{16}CO_3.4H_2O)$ , and show that NO<sub>3</sub>.Mg–Al LDH has an LDH structure. Table 1 lists the chemical composition of NO<sub>3</sub>·Mg-Al LDH. The molar ratios of Mg/Al and  $NO<sub>3</sub>/Al$  are 3.9 and 0.83, respectively. The Mg/Al molar ratio is similar to the expected value for the preparation procedure in this study. The  $NO<sub>3</sub>/Al$  molar ratio is 83% of the expected value, which is calculated from the neutralization of the positive charge of the Al-bearing brucite-like octahedral layers. This suggests that the  $NO_3^-$  content in  $NO_3$  Mg–Al LDH is governed by the charge balance in Mg–Al LDH. Accordingly,  $\rm NO_3^-$ -intercalated Mg–Al LDH was confirmed to be prepared by the co-precipitation method.

## 3.2. Thermal properties of  $NO<sub>3</sub>$ ·Mg-Al LDH

Recently, Frost et al. have aggressively examined the thermal decompositions of many kinds of LDHs such as  $CO<sub>3</sub>$ ·Mg-Al LDH, VO4·Mg–Al LDH, MoO4·Mg–Al LDH, AsO4·Mg–Al LDH, PO4·Mg–Al LDH, CO<sub>3</sub>·Mg-(Fe,Al) LDH, CO<sub>3</sub>·Mg-(Fe,Cr) LDH, CO<sub>3</sub>·Cu-Al LDH, and  $CO<sub>3</sub>$  Zn–Al LDH [13–18]. Frost's review presents that the thermal decomposition of CO3·Mg–Al LDH, which is the representative LDH, occurs in three steps: (i) removal of adsorbed water, (ii) elimination of the interlayer structural water, and (iii) the simultaneous dehydroxylation and decarbonation of the hydrotalcite framework [19]. Co[mpared](#page-4-0) [to](#page-4-0) these results, thermal properties of NO<sub>3</sub>·Mg-Al LDH were analyzed as follows.





<span id="page-2-0"></span>

Fig. 3. TG and DTG curves for NO<sub>3</sub> Mg-Al LDH.

Fig. 3 shows the TG and differential thermal gravimetry (DTG) curves obtained for  $NO<sub>3</sub> \cdot Mg-Al$  LDH. Decomposition of  $NO<sub>3</sub> \cdot Mg-Al$ LDH occurred in the following four stages: stage 1, mass loss of 0–8% until 120 ◦C; stage 2, mass loss of 8–26% at 120–350 ◦C; stage 3, mass loss of  $26-31\%$  at  $350-380$  °C; and stage 4, mass loss of 26–45% above 380 °C. The first stage corresponded to the evaporation of surface adsorbed water and interlayer water in  $NO<sub>3</sub>·Mg-Al$ LDH. The second and third stages were mainly attributable to the dehydroxylation of the brucite-like octahedral layers in  $NO<sub>3</sub>·Mg-Al$ LDH. The fourth stage was most probably due to the elimination of NO $_3^-$  intercalated in the Mg–Al LDH interlayers. Fig. 4 shows the TG curves obtained for  $NO<sub>3</sub>·Mg-Al$  LDH and the mass spectra of selected ions from among the major thermal decomposition products of  $NO<sub>3</sub>$ ·Mg-Al LDH. The mass spectrum showed signals at  $m/z$  18, 30, 32, 44, and 46, which corresponded to the molecular ion peaks of  $H_2O^+$ , NO<sup>+</sup>, O<sub>2</sub><sup>+</sup>, CO<sub>2</sub><sup>+</sup>, and NO<sub>2</sub><sup>+</sup>, respectively. The  $H_2O^+$  peak in the spectrum showed that  $H_2O$  was produced at four steps, i.e., during the elimination of surface adsorbed water and interlayer water (stage 1), dehydroxylation of  $NO<sub>3</sub>·Mg-Al$  LDH components whose properties were similar to those of  $Al(OH)_3$ and  $Mg(OH)_2$  (stages 2 and 3, respectively), and dehydroxylation of  $NO<sub>3</sub>$ ·Mg–Al LDH components whose properties were similar to those of Al(OH)<sub>3</sub> (stage 4) [20]. The NO<sup>+</sup> and NO<sub>2</sub><sup>+</sup> peaks were



Fig. 4. TG curve of NO<sub>3</sub> · Mg-Al LDH and selected-ion mass spectra of major products formed in thermal decomposition of NO3·Mg–Al LDH.



**Fig. 5.** Gibbs free energy change ( $\Delta G$ ) for the decomposition of Mg(OH)<sub>2</sub> and  $Mg(NO<sub>3</sub>)<sub>2</sub>$ .

observed at 300–600 ◦C and 350–500 ◦C in themass spectra, respectively (Fig. 4). The intensities of the NO<sup>+</sup> and NO<sub>2</sub><sup>+</sup> peaks were high in the fourth decomposition stage ( $>380$  °C), confirming that the mass loss of NO<sub>3</sub>·Mg-Al LDH in this stage was due to the formation of nitrogen oxides by the elimination of intercalated NO3 $^{\rm -}.$ The  $NO_2^+$  peak definitely corresponds to the occurrence of  $NO_2$ . The NO<sup>+</sup> peak generally corresponds to the occurrence of NO and  $NO<sub>2</sub>$ . However, the  $NO<sup>+</sup>$  peak in this study probably suggests the main formation of  $NO<sub>2</sub>$ , because the evolved nitrogen oxides by the thermal decomposition of  $Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O$  were observed to be only  $NO<sub>2</sub>$  in the TG-FTIR spectroscopy despite the presence of the  $m/z = 30$  ion fragment in TG–MS [21]. This is also supported by the fact that the  $m/z = 30$  ion fragment is the most intense fragment of  $NO<sub>2</sub>$  gas according to the reference mass spectra in NIST database [22]. Therefore, the elimination of  $\rm NO_3^-$  intercalated in the interlayer of  $NO<sub>3</sub>$ ·Mg–Al LDH during the thermal decomposition is certainl[y](#page-4-0) caused by [the](#page-4-0) [m](#page-4-0)ain formation of  $NO<sub>2</sub>$ . A prominent  $O_2$ <sup>+</sup> peak corresponding to the production of  $O_2$  was observed at 400–500 $\degree$ C. This is probably derived from the decomposition [of](#page-4-0)  $NO_3^ NO_3^-$  in  $NO_3$ ·Mg–Al LDH in the fourth decomposition stage (>380 $\degree$ C). The decomposition pattern of NO<sub>3</sub>·Mg-Al LDH is determined thermodynamically as follows. The thermal properties of  $NO<sub>3</sub>·Mg–Al LDH$  are assumed to resemble those of  $Mg(OH)<sub>2</sub>$  and Mg(NO<sub>3</sub>)<sub>2</sub>. Therefore, the Gibbs free energy change ( $\Delta G$ ) for the decomposition of  $Mg(OH)_2$  and  $Mg(NO_3)_2$  (shown in Eqs. (4) and (5)) is determined using the thermochemical data reported by Binnewies and Milke [23], as shown in Fig. 5:

$$
Mg(OH)_2 \rightarrow MgO + H_2O \tag{4}
$$

$$
Mg(NO_3)_2 \to MgO + 2NO_2 + (1/2)O_2 \tag{5}
$$

In t[he](#page-4-0) [dec](#page-4-0)omposition of  $Mg(OH)_2$  and  $Mg(NO_3)_2$ , the temperatures corresponding to  $\Delta G$  < 0 were found to exceed 269 and 366 °C, respectively. This implied that the decomposition of  $NO<sub>3</sub>$ ·Mg-Al LDH was thermodynamically favorable, resulting in the production of  $H_2O$  and  $NO_2$ . In fact, the temperature for  $H_2O$  production from the dehydroxylation of NO<sub>3</sub>·Mg-Al LDH was lower than that for NO2 production (Fig. 4). This result was in good agreement with the thermodynamic consideration that the temperature for  $Mg(OH)_2$ decomposition is lower than that for  $Mg(NO<sub>3</sub>)<sub>2</sub>$  decomposition. By the way, a CO $_2^{\text{+}}$  peak, which corresponded to the formation of CO $_2$ , was observed at  $250-400$  °C in the mass spectrum (Fig. 4), indicating the elimination of  $CO<sub>2</sub>$  from NO<sub>3</sub> Mg-Al LDH. As shown in Table 1, the  $NO<sub>3</sub>/Al$  molar ratio in the  $NO<sub>3</sub>·Mg-Al$  LDH was lower than 1.0, suggesting that CO<sub>3</sub><sup>2–</sup> in addition to NO<sub>3</sub><sup>–</sup> was intercalated in the interlayer of Mg–Al LDH in order to compensate the

<span id="page-3-0"></span>



**Fig. 6.** Variation in the elimination of nitrogen oxides with time in the thermal decomposition of NO<sub>3</sub>⋅Mg-Al LDH at 400 °C.

positive charge of the Al-bearing brucite-like octahedral layers. This contamination by CO<sub>3</sub><sup>2−</sup> is due to the dissolution of CO<sub>2</sub> into the solution in the preparation procedure. The elimination of  $CO<sub>2</sub>$  certainly does not affect the production of  $NO<sub>2</sub>$ . Fig. 4 also presents that  $CO_2^+$  and  $H_2O^+$  peaks were observed at 250–400 $\degree$ C, respectively, supporting the simultaneous dehydroxylation and decarbonation of the  $CO_3$ ·Mg–Al LDH, as mentioned by Frost's review [19]. In case of NO<sub>3</sub>·Mg–Al LDH, the dehydroxylation and elimination of NO<sub>3</sub> $^$ were found to occur differently, [confirm](#page-2-0)ed by the fact that the NO<sup>+</sup> and NO $_2^+$  peaks were mainly observed at around 400–500  $^\circ$ C in the mass spectra, respectively (Fig. 4).

To summarize, the decomposition of NO<sub>3</sub> Mg-Al LDH proceeded in four stages. Stage 1: evaporation of surface adsorbed water and interlayer water in  $NO<sub>3</sub>$ ·Mg-Al LDH; stages 2 and 3: dehydroxylation of the brucite-like octahedral layers in  $NO<sub>3</sub>·Mg-Al$  LDH; and stage 4: eli[minatio](#page-2-0)n of NO $_3^-$  intercalated in the Mg–Al LDH interlayers to afford  $NO<sub>2</sub>$ .

## 3.3. Elimination behavior of nitrogen oxides from  $NO<sub>3</sub>·Mg-Al$  LDH

In this section, we report the elimination behavior of nitrogen oxides from  $NO<sub>3</sub>·Mg-Al$  LDH estimated using the experimental apparatus shown in Fig. 2 and the production of Mg–Al oxide. Fig. 6 shows the variation in the elimination of nitrogen oxides with time during the thermal decomposition of  $NO<sub>3</sub>·Mg-Al$  LDH at 400 $°C$ . Since  $N\rm O_2^-$  and  $N\rm O_3^-$  are detected in the water traps, the elimination of nitrogen oxides is expressed as the ratio of the mole percent of  $NO_2^ NO_2^-$  [and](#page-1-0)  $NO_3^-$  in the traps to that of  $NO_3^-$  in  $NO_3 \cdot Mg$ –Al LDH. The elimination of nitrogen oxides increases with time, reaching 91.7% in 180 min. The solutions in the traps are strongly acidic, thus confirming the production of  $HNO<sub>3</sub>$  and  $HNO<sub>2</sub>$ . The thermal decomposition of NO<sub>3</sub>·Mg-Al LDH results in the main formation of  $NO<sub>2</sub>$ . NO<sub>2</sub> then reacts with H<sub>2</sub>O and O<sub>2</sub> to form HNO<sub>3</sub> and HNO<sub>2</sub> in the manner shown in Eqs. (6) and (7), respectively [24,25].

$$
2NO2 + H2O \rightarrow HNO3 + HNO2
$$
 (6)

$$
2NO2 + H2O + (1/2)O2 \rightarrow 2HNO3
$$
 (7)

As shown in Fig. 6, the elimination for NO3 $^{\mathrm{-}}$  [is](#page-4-0) [co](#page-4-0)nsiderably higher than that for NO $_2^-$  at any given instant. This indicates that the production of  $HNO<sub>3</sub>$  is mainly caused by the reaction shown in Eq. (7).

Fig. 7 shows the effect of temperature on the elimination of nitrogen oxides in the thermal decomposition of NO<sub>3</sub>·Mg-Al LDH. At  $400^{\circ}$ C, the elimination of nitrogen oxides increased gradually with time, reaching 78.9% in 60 min. At 500 and 600 ℃, the elimination of nitrogen oxides increased rapidly with time, reaching

**Fig. 7.** Effect of temperature on the elimination of nitrogen oxides in the thermal decomposition of NO3·Mg–Al LDH.

100% within 30 and 15 min, respectively. The elimination of nitrogen oxides was thus confirmed to increase with temperature as well. Notably, all the intercalated  $NO_3^-$  was lost from  $NO_3$  Mg–Al LDH at 500 and 600 °C, and this explained why the  $\rm NO_2^+$  and  $\rm NO^+$ peaks could not be detected in the mass spectrum at temperatures above 500 and 600 $\degree$ C, respectively (Fig. 4). Fig. 8 presents the XRD patterns for the products obtained in the thermal decomposition of NO3·Mg–Al LDH under different heating conditions. Although the product obtained at 1100 ◦C after 180 min was a mixture of MgO and  $MgAl<sub>2</sub>O<sub>4</sub>$ , only Mg-Al oxide was obtained under other conditions. Thus, it could be c[onfirme](#page-2-0)d that the thermal decomposition of NO3·Mg–Al LDH at 400–600 ◦C results in the formation of Mg–Al oxide only.



**Fig. 8.** XRD patterns for products obtained in the thermal decomposition of NO3·Mg–Al LDH under different heating conditions: (a) 400 ◦C, 15 min; (b) 500 ◦C, 15 min; (c) 600 ◦C, 15 min; (d) 600 ◦C, 60 min; and (e) 1100 ◦C, 180 min.

<span id="page-4-0"></span>**Table 2** Degree of  $NO_3^-$  removal from HNO<sub>3</sub> solution by Mg–Al oxides obtained with various temperatures.

Temperature/ $\degree$ C	$NO_3$ <sup>-</sup> removal/%
400	52.5
500	78.0
600	65.3

## 3.4. Treatment of HNO<sub>3</sub>

Fig. 7 presents the highest eliminations of nitrogen oxides at 400 °C for 60 min, at 500 °C for 30 min, and at 600 °C for 15 min, respectively. Mg–Al oxides, converted from  $NO<sub>3</sub>$ ·Mg–Al LDHs with these conditions, were examined to treat  $HNO<sub>3</sub>$ . Table 2 shows the degree of NO $_3^-$  removal from HNO $_3$  solution by the Mg–Al oxides. All Mg–Al oxides were able to remove  $\rm NO_3^-$  from  $\rm HNO_3$ solution. As shown in Fig. 7, some  $NO_3^-$  is remained in Mg–Al oxide obtained at 400 °C for 60 min. The remaining of NO<sub>3</sub>  $^-$  leads to the lowest degree of NO3 $^-$  removal for Mg–Al oxide obtained at 400 °C. The degree of NO<sub>3</sub>– removal for 500 °C was higher than that for 600 °[C, altho](#page-3-0)ugh NO $_3^-$  was completely lost in Mg–Al oxides obtained at both temperatures. The high temperature probably promotes the crystallization of Mg–Al oxide for the conversion to MgO and  $MgAl<sub>2</sub>O<sub>4</sub>$ . This crystallization likely results in the decrease of  $\rm NO_3^-$  removal capability.

## **4. Conclusions**

The thermal decomposition of  $NO<sub>3</sub>·Mg-Al$  LDH occurred in the following four stages: evaporation of surface adsorbed water and interlayer water (stage 1), dehydroxylation of the brucite-like octahedral layers in  $NO<sub>3</sub>·Mg-Al$  LDH (stages 2 and 3), and elimination of NO $_3^-$  intercalated in the Mg–Al LDH interlayers to afford NO $_2$  (stage 4). The thermal properties of  $NO<sub>3</sub>$  Mg-Al LDH were considered to be similar to those of  $Mg(OH)_2$  and  $Mg(NO_3)_2$ . The temperature for  $H_2O$  formation from the dehydroxylation of  $NO_3 \cdot Mg-Al$ LDH was lower than that for  $NO<sub>2</sub>$  production. This observation was consistent with the thermodynamic consideration that the temperature for  $Mg(OH)_2$  decomposition is lower than that for  $Mg(NO_3)_2$ decomposition.  $NO<sub>2</sub>$ , which was produced by the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH at 400–600 $\degree$ C, reacted with H<sub>2</sub>O and

 $O<sub>2</sub>$  to form HNO<sub>3</sub> and HNO<sub>2</sub>. The elimination of nitrogen oxides was found to increase with the decomposition time and temperature. Further, all the intercalated NO3 $^-$  was completely eliminated from NO<sub>3</sub>·Mg–Al LDH at 500 and 600 °C, confirming that Mg–Al oxide was produced upon the thermal decomposition of  $NO<sub>3</sub>$ ·Mg-Al LDH at 400–600 $\degree$ C. The Mg–Al oxide was able to treat HNO<sub>3</sub> solution. To summarize, complete loss of nitrogen oxides of  $NO<sub>3</sub>·Mg-Al$  LDH and formation of Mg–Al oxide occurred in the thermal decomposition of  $NO<sub>3</sub>·Mg-Al$  LDH. On the basis of the present results, we concluded that cyclic usage of Mg–Al oxide for the treatment of  $HNO<sub>3</sub>$  is possible.

## **References**

- [1] F. Cavani, F. Trifiro, A. Vaccari, Catal. Today 11 (1991) 173.
- [2] S.P. Newman, W. Jones, New J. Chem. 22 (1998) 105.
- [3] A.D. Roy, Mol. Cryst. Liq. Cryst. 311 (1998) 173.
- [4] Y. You, G.F. Vance, H. Zhao, Appl. Clay Sci. 20 (2001) 13.
- [5] M.Z. Hussein, Z. Zainal, I. Yaziz, T.C. Beng, J. Environ. Sci. Health A 36 (2001) 565.
- [6] B. Dousova, V. Machovic, D. Kolousek, F. Kovanda, V. Dornicak, Water Air Soil Pollut. 149 (2003) 251.
- [7] L.P. Cardoso, J. Tronto, E.L. Crepaldi, J.B. Valim, Mol. Cryst. Liq. Cryst. 390 (2003) 49.
- [8] F. Li, Y. Wang, Q. Yang, D.G. Evans, C. Forano, X. Duan, J. Hazard. Mater. B125 (2005) 89.
- [9] S. Miyata, Clays Clay Miner. 31 (1983) 305.
- [10] L. Ingram, H.F.W. Taylor, Miner. Mag. 36 (1967) 465.
- [11] R. Allmann, Acta Cryst. B24 (1968) 972.
- [12] T. Kameda, F. Yabuuchi, T. Yoshioka, M. Uchida, A. Okuwaki, Water Res. 37 (2003) 1545.
- [13] R.L. Frost, A.W. Musumeci, M.O. Adebajo, W. Martens, J. Therm. Anal. Calorim. 89 (2007) 95.
- [14] S.J. Palmer, R.L. Frost, T. Nguyen, J. Therm. Anal. Calorim. 92 (2008) 879.
- [15] H.J. Spratt, S.J. Palmer, R.L. Frost, Thermochim. Acta 479 (2008) 1.
- [16] R.L. Frost, A. Soisnard, N. Voyer, S.J. Palmer, W.N. Martens, J. Raman Spectrosc. 40 (2009) 645.
- S.J. Palmer, A. Soisnard, R.L. Frost, J. Colloid Interface Sci. 329 (2009) 404.
- [18] S.J. Palmer, H.J. Spratt, R.L. Frost, J. Therm. Anal. Calorim. 95 (2009) 123.
- [19] S.J. Palmer, R.L. Frost, T. Nguyen, Coord. Chem. Rev. 253 (2009) 250.
- [20] T. Kameda, T. Yoshioka, K. Watanabe, M. Uchida, A. Okuwaki, Appl. Clay Sci. 35 (2007) 173.
- [21] J. Madarasz, P.P. Varga, G. Pokol, J. Anal. Appl. Pyrol. 79 (2007) 475.
- [22] NIST Chemistry Webbook Standard Reference Database, No. 69, June 2005 Release. http://www.webbook.nist.gov/chemistry.
- [23] M. Binnewies, E. Milke, Wiley-VCH Verlag GmbH, Thermochemical Data of Elements and Compound, 2nd edn. Weinheim, 2002.
- [24] F.S. Chambers, T.K. Sherwood, Ind. Eng. Chem. 29 (1937) 1415.
- [25] M.S. Peters, C.P. Ross, J.E. Klein, AIChE J. 1 (1955) 105.