Contents lists available at ScienceDirect





Thermochimica Acta

journal homepage: www.elsevier.com/locate/tca

# Elimination behavior of nitrogen oxides from a NO<sub>3</sub><sup>-</sup>-intercalated Mg–Al layered double hydroxide during thermal decomposition

# Tomohito Kameda\*, Yuki Fubasami, Naoya Uchiyama, Toshiaki Yoshioka

Graduate School of Environmental Studies, Tohoku University, 6-6-07 Aoba, Aramaki, Aoba-ku, Sendai 980-8579, Japan

#### ARTICLE INFO

Article history: Received 19 August 2009 Received in revised form 11 November 2009 Accepted 17 November 2009 Available online 24 November 2009

Keywords: Elimination Nitrogen oxides Mg-Al layered double hydroxide Thermal decomposition TG-MS

# 1. Introduction

It has been found that Mg–Al layered double hydroxide (Mg–Al LDH) can be used as an adsorbent for the removal of anionic pollutants in aqueous media [1–8]. Mg–Al LDH can be used as an anion exchanger [9] and is represented by the formula  $[Mg^{2+}_{1-x}Al^{3+}_x(OH)_2](A^{n-})_{x/n}\cdotmH_2O$ , where  $A^{n-}$  is an anion such as  $CO_3^{2-}$  and  $Cl^-$ , and x is the Al/(Mg + Al) molar ratio ( $0.20 \le x \le 0.33$ ) [10,11]. Mg–Al LDH consists of brucite-like octahedral layers that are positively charged because of the replacement of some Mg<sup>2+</sup> units by Al<sup>3+</sup>, while the interlayer anions help in maintaining charge balance. Water (H<sub>2</sub>O) molecules occupy the remaining spaces in the interlayer.  $CO_3^{2-}$ -intercalated Mg–Al LDH ( $CO_3\cdotMg$ –Al LDH) can be converted to Mg–Al oxide by calcination at 450–800 °C. The formation of Mg–Al oxide is represented by the following reaction:

$$Mg_{1-x}Al_x(OH)_2(CO_3)_{x/2} \rightarrow Mg_{1-x}Al_xO_{1+x/2} + (x/2)CO_2 + H_2O$$
 (1)

The resulting Mg–Al oxide undergoes rehydration and combines with anions to afford the original LDH structure, as shown in the following equation:

$$Mg_{1-x}Al_{x}O_{1+x/2} + x/nA^{n-} + (1+x/2)H_{2}O$$
  

$$\rightarrow Mg_{1-x}Al_{x}(OH)_{2}A_{x/n} + xOH^{-}$$
(2)

# ABSTRACT

The thermal properties of NO<sub>3</sub><sup>-</sup>-intercalated Mg–Al layered double hydroxide (NO<sub>3</sub>·Mg–Al LDH) were investigated using simultaneous thermogravimetry–mass spectrometry (TG–MS), and the elimination behavior of nitrogen oxides from this double hydroxide was examined. The TG–MS results showed that NO<sub>3</sub>·Mg–Al LDH decomposed in four stages. The first stage involved evaporation of surface adsorbed water and interlayer water in NO<sub>3</sub>·Mg–Al LDH. In the second and third stages, dehydroxylation of the brucite-like octahedral layers in NO<sub>3</sub>·Mg–Al LDH occurred. The fourth stage mainly corresponded to the elimination of NO<sub>3</sub><sup>-</sup> intercalated in the Mg–Al LDH interlayers to afford NO<sub>2</sub>. Thermal decomposition of NO<sub>3</sub>·Mg–Al LDH at 400–600 °C resulted in the formation of Mg–Al oxide, and the produced NO<sub>2</sub> reacted with H<sub>2</sub>O and O<sub>2</sub> to form HNO<sub>3</sub> and HNO<sub>2</sub>. The elimination of nitrogen oxides was found to increase with time and decomposition temperature. The synthesized Mg–Al oxide mixture could be used to remove nitric acid from aqueous solutions.

© 2009 Elsevier B.V. All rights reserved.

The abovementioned rehydration and subsequent combination of Mg–Al oxide with anions in solution are accompanied by the release of OH<sup>-</sup>. Accordingly, Mg–Al oxide can neutralize and fix NO<sub>3</sub><sup>-</sup> when used in the treatment of HNO<sub>3</sub> [12]. Subsequently, NO<sub>3</sub><sup>-</sup>-intercalated Mg–Al LDH (NO<sub>3</sub>·Mg–Al LDH) is produced by the reconstruction of Mg–Al oxide. In actual wastewater treatment, large quantities of Mg–Al oxide are used, and hence, considerable amounts of waste NO<sub>3</sub>·Mg–Al LDH are generated. If Mg–Al oxide can be regenerated from the obtained NO<sub>3</sub>·Mg–Al LDH and reused to treat waste HNO<sub>3</sub>, the energy required for the synthesis of Mg–Al oxide and CO<sub>3</sub>·Mg–Al LDH will be drastically reduced, and the formation of NO<sub>3</sub>·Mg–Al LDH wastes can be prevented. In order to effectively reuse Mg–Al oxide for the treatment of HNO<sub>3</sub>, it is necessary to examine in detail the thermal decomposition behavior of NO<sub>3</sub>·Mg–Al LDH and the elimination of nitrogen oxides.

In this study, we investigated the thermal properties of  $NO_3 \cdot Mg$ -Al LDH by simultaneous thermogravimetry-mass spectrometry (TG-MS). In addition, we carried out thermal decomposition of  $NO_3 \cdot Mg$ -Al LDH in air and investigated the effect of temperature on its elimination behavior of nitrogen oxides. We also examined the capability for the treatment of HNO<sub>3</sub> with Mg-Al oxides obtained by the thermal decomposition of  $NO_3 \cdot Mg$ -Al LDHs at different temperature.

# 2. Experimental

# 2.1. Preparation

 $NO_3\cdot Mg-Al$  LDH was prepared by the co-precipitation method. The Mg-Al solution (0.4 M  $Mg(NO_3)_2$  + 0.1 M  $Al(NO_3)_3$ ) was pre-

<sup>\*</sup> Corresponding author. Tel.: +81 22 795 7212; fax: +81 22 795 7212. *E-mail address:* kameda@env.che.tohoku.ac.jp (T. Kameda).

<sup>0040-6031/\$ –</sup> see front matter s 2009 Elsevier B.V. All rights reserved. doi:10.1016/j.tca.2009.11.009



**Fig. 1.** Experimental apparatus used for thermal decomposition of NO<sub>3</sub>·Mg–Al LDH. (1) Air cylinder; (2) flow meter; (3) thermocouple; (4) sample; (5) electric furnace; (6) quartz reaction tube; (7) aluminum boat; (8) flexible heater; and (9) water trap  $(0 \,^{\circ}$ C).

pared by dissolving Mg(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O (0.1 mol) and Al(NO<sub>3</sub>)<sub>3</sub>.9H<sub>2</sub>O (0.025 mol) in 250 mL of deionized water. The Mg-Al solution was added dropwise to 250 mL of 0.3 mM NaOH solution at 30 °C with mild agitation. The solution pH was adjusted to 10.5 by adding 0.5 M NaOH solution. The mixture was then stirred continuously at 30 °C for 1 h. The NO<sub>3</sub>·Mg-Al LDH that formed was isolated by filtering the resulting suspension, washing it thoroughly with deionized water, and drying it under reduced pressure (133 Pa) at 40 °C for 40 h. The NO<sub>3</sub> Mg-Al LDH crystals were ground into powder using a mortar and pestle, and the resulting powder was characterized by X-ray diffraction (XRD) using a Rigaku RINT-2200VHF diffractometer (Rigaku Corp., Tokyo, Japan) with CuKa radiation at 40 kV and 20 mA (scan rate: 2° min<sup>-1</sup>). The NO<sub>3</sub> Mg-Al LDH was dissolved in 1 M HNO<sub>3</sub>, and analyzed for Mg<sup>2+</sup> and Al<sup>3+</sup> using inductively coupled plasma-atomic emission spectrometry (ICP-AES). The NO3 Mg-Al LDH was also dissolved in 0.1 M HCl, and analyzed for NO<sub>3</sub><sup>-</sup> using a Dionex DX-120 ion chromatograph equipped with an AS-12A column (eluent: 2.7 mM Na<sub>2</sub>CO<sub>3</sub> and 0.3 mM NaHCO<sub>3</sub>; flow rate:  $1.3 \text{ mLmin}^{-1}$ ).

# 2.2. Thermal properties of NO<sub>3</sub>·Mg–Al LDH

A 10-mg sample of NO<sub>3</sub>·Mg–Al LDH was analyzed by simultaneous TG (Seiko Instruments TG/DTA 6200) and MS (Hewlett Packard 5973) at a heating rate of  $5 \,^{\circ}$ C min<sup>-1</sup> in a He flow rate of 200 mL min<sup>-1</sup>. The decomposition products were introduced to the MS ion source through an inactivated stainless steel capillary tube heated at 300 °C to prevent condensation of the evolved products.

# 2.3. Elimination behavior of nitrogen oxides from NO<sub>3</sub>·Mg-Al LDH

The experimental apparatus used for carrying out the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH is shown in Fig. 1. An aluminum boat containing 0.5 g of NO<sub>3</sub>·Mg–Al LDH was inserted in a quartz reaction tube, which was placed in an electric furnace. NO<sub>3</sub>·Mg–Al LDH decomposed at 400–600 °C at an air flow rate of 50 mL min<sup>-1</sup>. The evolved gas was collected in three water traps (0 °C) containing 30 mL deionized water. In order to prevent condensation of the evolved gas, the line from the quartz reaction tube to the trap was heated to 110–130 °C using a flexible heater. The anions in the traps were quantified using ion chromatograph. The products obtained in the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH were identified by XRD analysis.

# 2.4. Treatment of HNO<sub>3</sub>

Mg–Al oxides, obtained by the thermal decomposition of  $NO_3$ ·Mg–Al LDH at 400–600 °C using the experimental apparatus



Fig. 2. XRD patterns for NO<sub>3</sub>·Mg–Al LDH.

shown in Fig. 1, were examined to check the capability for the treatment of HNO<sub>3</sub>. 10 mL of 0.1 M HNO<sub>3</sub> solution were added to a pre-determined amount of  $Mg_{0.80}Al_{0.20}O_{1.10}$  in 50-mL screw-top tubes, and shaken at 25 °C for 24 h. The quantity of  $Mg_{0.80}Al_{0.20}O_{1.10}$  used was a stoichiometric quantity according to Eq. (3).

 $Mg_{0.80}Al_{0.20}O_{1.10} + 0.20HNO_3 + 0.90H_2O$ 

$$\rightarrow Mg_{0.80}Al_{0.20}(OH)_2(NO_3)_{0.20}$$
(3)

The NO<sub>3</sub><sup>-</sup> concentration of the filtrate was determined using the ion chromatograph.

#### 3. Results and discussion

#### 3.1. Preparation

The XRD patterns obtained for  $NO_3 \cdot Mg$ -Al LDH (Fig. 2) are ascribed to hydrotalcite (JCPDS card 22-700), a naturally occurring hydroxycarbonate of magnesium and aluminum  $(Mg_6Al_2(OH)_{16}CO_3 \cdot 4H_2O)$ , and show that  $NO_3 \cdot Mg$ -Al LDH has an LDH structure. Table 1 lists the chemical composition of  $NO_3 \cdot Mg$ -Al LDH. The molar ratios of Mg/Al and  $NO_3$ /Al are 3.9 and 0.83, respectively. The Mg/Al molar ratio is similar to the expected value for the preparation procedure in this study. The  $NO_3$ /Al molar ratio is 83% of the expected value, which is calculated from the neutralization of the positive charge of the Al-bearing brucite-like octahedral layers. This suggests that the  $NO_3^-$  content in  $NO_3 \cdot Mg$ -Al LDH is governed by the charge balance in Mg-Al LDH. Accordingly,  $NO_3^-$ -intercalated Mg-Al LDH was confirmed to be prepared by the co-precipitation method.

# 3.2. Thermal properties of NO<sub>3</sub>·Mg-Al LDH

Recently, Frost et al. have aggressively examined the thermal decompositions of many kinds of LDHs such as  $CO_3 \cdot Mg$ -Al LDH,  $VO_4 \cdot Mg$ -Al LDH,  $MO_4 \cdot Mg$ -Al LDH,  $AsO_4 \cdot Mg$ -Al LDH,  $PO_4 \cdot Mg$ -Al LDH,  $CO_3 \cdot Mg$ -(Fe,Al) LDH,  $CO_3 \cdot Mg$ -(Fe,Cr) LDH,  $CO_3 \cdot Cu$ -Al LDH, and  $CO_3 \cdot Zn$ -Al LDH [13–18]. Frost's review presents that the thermal decomposition of  $CO_3 \cdot Mg$ -Al LDH, which is the representative LDH, occurs in three steps: (i) removal of adsorbed water, (ii) elimination of the interlayer structural water, and (iii) the simultaneous dehydroxylation and decarbonation of the hydrotalcite framework [19]. Compared to these results, thermal properties of  $NO_3 \cdot Mg$ -Al LDH were analyzed as follows.

lable I		
Chemical	composition of NO3 · M	g–Al LDH.

Mass %			Molar ratio	
Mg	Al	NO <sub>3</sub>	Mg/Al	$NO_3/Al$
23.7	6.7	12.7	3.9	0.83



Fig. 3. TG and DTG curves for NO<sub>3</sub>·Mg–Al LDH.

Fig. 3 shows the TG and differential thermal gravimetry (DTG) curves obtained for NO3·Mg-Al LDH. Decomposition of NO3·Mg-Al LDH occurred in the following four stages: stage 1, mass loss of 0-8% until 120 °C; stage 2, mass loss of 8-26% at 120-350 °C; stage 3, mass loss of 26-31% at 350-380°C; and stage 4, mass loss of 26-45% above 380 °C. The first stage corresponded to the evaporation of surface adsorbed water and interlayer water in NO<sub>3</sub>·Mg-Al LDH. The second and third stages were mainly attributable to the dehydroxylation of the brucite-like octahedral layers in NO3 Mg-Al LDH. The fourth stage was most probably due to the elimination of NO<sub>3</sub><sup>-</sup> intercalated in the Mg-Al LDH interlayers. Fig. 4 shows the TG curves obtained for NO<sub>3</sub>·Mg-Al LDH and the mass spectra of selected ions from among the major thermal decomposition products of NO<sub>3</sub>·Mg-Al LDH. The mass spectrum showed signals at m/z 18, 30, 32, 44, and 46, which corresponded to the molecular ion peaks of  $H_2O^+$ ,  $NO^+$ ,  $O_2^+$ ,  $CO_2^+$ , and  $NO_2^+$ , respectively. The  $H_2O^+$  peak in the spectrum showed that  $H_2O$  was produced at four steps, i.e., during the elimination of surface adsorbed water and interlayer water (stage 1), dehydroxylation of NO<sub>3</sub>·Mg–Al LDH components whose properties were similar to those of Al(OH)<sub>3</sub> and Mg(OH)<sub>2</sub> (stages 2 and 3, respectively), and dehydroxylation of NO<sub>3</sub>·Mg-Al LDH components whose properties were similar to those of  $Al(OH)_3$  (stage 4) [20]. The NO<sup>+</sup> and NO<sub>2</sub><sup>+</sup> peaks were



**Fig. 4.** TG curve of  $NO_3 \cdot Mg$ -Al LDH and selected-ion mass spectra of major products formed in thermal decomposition of  $NO_3 \cdot Mg$ -Al LDH.



**Fig. 5.** Gibbs free energy change  $(\Delta G)$  for the decomposition of Mg(OH)<sub>2</sub> and Mg(NO<sub>3</sub>)<sub>2</sub>.

observed at 300-600 °C and 350-500 °C in the mass spectra, respectively (Fig. 4). The intensities of the  $NO^+$  and  $NO_2^+$  peaks were high in the fourth decomposition stage (>380 °C), confirming that the mass loss of NO<sub>3</sub>·Mg-Al LDH in this stage was due to the formation of nitrogen oxides by the elimination of intercalated NO<sub>3</sub><sup>-</sup>. The  $NO_2^+$  peak definitely corresponds to the occurrence of  $NO_2$ . The NO<sup>+</sup> peak generally corresponds to the occurrence of NO and NO<sub>2</sub>. However, the NO<sup>+</sup> peak in this study probably suggests the main formation of NO<sub>2</sub>, because the evolved nitrogen oxides by the thermal decomposition of  $Mg(NO_3)_2 \cdot 6H_2O$  were observed to be only NO<sub>2</sub> in the TG-FTIR spectroscopy despite the presence of the m/z = 30 ion fragment in TG-MS [21]. This is also supported by the fact that the m/z = 30 ion fragment is the most intense fragment of NO<sub>2</sub> gas according to the reference mass spectra in NIST database [22]. Therefore, the elimination of NO<sub>3</sub><sup>-</sup> intercalated in the interlayer of NO<sub>3</sub>·Mg–Al LDH during the thermal decomposition is certainly caused by the main formation of NO<sub>2</sub>. A prominent  $O_2^+$  peak corresponding to the production of  $O_2$  was observed at 400–500 °C. This is probably derived from the decomposition of NO<sub>3</sub><sup>-</sup> in NO<sub>3</sub>·Mg-Al LDH in the fourth decomposition stage (>380 °C). The decomposition pattern of NO<sub>3</sub>·Mg–Al LDH is determined thermodynamically as follows. The thermal properties of NO<sub>3</sub>·Mg-Al LDH are assumed to resemble those of Mg(OH)<sub>2</sub> and  $Mg(NO_3)_2$ . Therefore, the Gibbs free energy change ( $\Delta G$ ) for the decomposition of Mg(OH)<sub>2</sub> and Mg(NO<sub>3</sub>)<sub>2</sub> (shown in Eqs. (4) and (5)) is determined using the thermochemical data reported by Binnewies and Milke [23], as shown in Fig. 5:

$$Mg(OH)_2 \rightarrow MgO + H_2O \tag{4}$$

$$Mg(NO_3)_2 \rightarrow MgO + 2NO_2 + (1/2)O_2$$
 (5)

In the decomposition of Mg(OH)<sub>2</sub> and Mg(NO<sub>3</sub>)<sub>2</sub>, the temperatures corresponding to  $\Delta G < 0$  were found to exceed 269 and 366 °C, respectively. This implied that the decomposition of NO<sub>3</sub>·Mg–Al LDH was thermodynamically favorable, resulting in the production of H<sub>2</sub>O and NO<sub>2</sub>. In fact, the temperature for H<sub>2</sub>O production from the dehydroxylation of NO<sub>3</sub>·Mg–Al LDH was lower than that for NO<sub>2</sub> production (Fig. 4). This result was in good agreement with the thermodynamic consideration that the temperature for Mg(OH)<sub>2</sub> decomposition is lower than that for Mg(NO<sub>3</sub>)<sub>2</sub> decomposition. By the way, a CO<sub>2</sub><sup>+</sup> peak, which corresponded to the formation of CO<sub>2</sub>, was observed at 250–400 °C in the mass spectrum (Fig. 4), indicating the elimination of CO<sub>2</sub> from NO<sub>3</sub>·Mg–Al LDH was lower than 1.0, suggesting that CO<sub>3</sub><sup>2–</sup> in addition to NO<sub>3</sub><sup>-</sup> was intercalated in the interlayer of Mg–Al LDH in order to compensate the



Fig. 6. Variation in the elimination of nitrogen oxides with time in the thermal decomposition of  $NO_3$ -Mg–Al LDH at 400 °C.

positive charge of the Al-bearing brucite-like octahedral layers. This contamination by  $CO_3^{2-}$  is due to the dissolution of  $CO_2$  into the solution in the preparation procedure. The elimination of  $CO_2$  certainly does not affect the production of  $NO_2$ . Fig. 4 also presents that  $CO_2^+$  and  $H_2O^+$  peaks were observed at 250–400 °C, respectively, supporting the simultaneous dehydroxylation and decarbonation of the  $CO_3 \cdot Mg$ –Al LDH, as mentioned by Frost's review [19]. In case of  $NO_3 \cdot Mg$ –Al LDH, the dehydroxylation and elimination of  $NO_3^-$  were found to occur differently, confirmed by the fact that the  $NO^+$  and  $NO_2^+$  peaks were mainly observed at around 400–500 °C in the mass spectra, respectively (Fig. 4).

To summarize, the decomposition of NO<sub>3</sub>·Mg–Al LDH proceeded in four stages. Stage 1: evaporation of surface adsorbed water and interlayer water in NO<sub>3</sub>·Mg–Al LDH; stages 2 and 3: dehydroxylation of the brucite-like octahedral layers in NO<sub>3</sub>·Mg–Al LDH; and stage 4: elimination of NO<sub>3</sub><sup>-</sup> intercalated in the Mg–Al LDH interlayers to afford NO<sub>2</sub>.

#### 3.3. Elimination behavior of nitrogen oxides from NO<sub>3</sub>·Mg-Al LDH

In this section, we report the elimination behavior of nitrogen oxides from NO<sub>3</sub>·Mg–Al LDH estimated using the experimental apparatus shown in Fig. 2 and the production of Mg–Al oxide. Fig. 6 shows the variation in the elimination of nitrogen oxides with time during the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH at 400 °C. Since NO<sub>2</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> are detected in the water traps, the elimination of nitrogen oxides is expressed as the ratio of the mole percent of NO<sub>2</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> in the traps to that of NO<sub>3</sub><sup>-</sup> in NO<sub>3</sub>·Mg–Al LDH. The elimination of nitrogen oxides increases with time, reaching 91.7% in 180 min. The solutions in the traps are strongly acidic, thus confirming the production of HNO<sub>3</sub> and HNO<sub>2</sub>. The thermal decomposition of NO<sub>3</sub>·Mg–Al LDH results in the main formation of NO<sub>2</sub>. NO<sub>2</sub> then reacts with H<sub>2</sub>O and O<sub>2</sub> to form HNO<sub>3</sub> and HNO<sub>2</sub> in the manner shown in Eqs. (6) and (7), respectively [24,25].

$$2NO_2 + H_2O \rightarrow HNO_3 + HNO_2 \tag{6}$$

$$2NO_2 + H_2O + (1/2)O_2 \to 2HNO_3$$
(7)

As shown in Fig. 6, the elimination for  $NO_3^-$  is considerably higher than that for  $NO_2^-$  at any given instant. This indicates that the production of  $HNO_3$  is mainly caused by the reaction shown in Eq. (7).

Fig. 7 shows the effect of temperature on the elimination of nitrogen oxides in the thermal decomposition of  $NO_3 \cdot Mg$ -Al LDH. At 400 °C, the elimination of nitrogen oxides increased gradually with time, reaching 78.9% in 60 min. At 500 and 600 °C, the elimination of nitrogen oxides increased rapidly with time, reaching



**Fig. 7.** Effect of temperature on the elimination of nitrogen oxides in the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH.

100% within 30 and 15 min, respectively. The elimination of nitrogen oxides was thus confirmed to increase with temperature as well. Notably, all the intercalated  $NO_3^-$  was lost from  $NO_3 \cdot Mg$ -Al LDH at 500 and 600 °C, and this explained why the  $NO_2^+$  and  $NO^+$  peaks could not be detected in the mass spectrum at temperatures above 500 and 600 °C, respectively (Fig. 4). Fig. 8 presents the XRD patterns for the products obtained in the thermal decomposition of  $NO_3 \cdot Mg$ -Al LDH under different heating conditions. Although the product obtained at 1100 °C after 180 min was a mixture of MgO and MgAl<sub>2</sub>O<sub>4</sub>, only Mg-Al oxide was obtained under other conditions. Thus, it could be confirmed that the thermal decomposition of  $NO_3 \cdot Mg$ -Al LDH at 400–600 °C results in the formation of Mg-Al oxide only.



**Fig. 8.** XRD patterns for products obtained in the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH under different heating conditions: (a) 400 °C, 15 min; (b) 500 °C, 15 min; (c) 600 °C, 15 min; (d) 600 °C, 60 min; and (e) 1100 °C, 180 min.

 Table 2

 Degree of NO<sub>3</sub><sup>-</sup> removal from HNO<sub>3</sub> solution by Mg–Al oxides obtained with various temperatures.

Temperature/°C	NO3- removal/%	
400	52.5	
500	78.0	
600	65.3	

#### 3.4. Treatment of HNO<sub>3</sub>

Fig. 7 presents the highest eliminations of nitrogen oxides at 400 °C for 60 min, at 500 °C for 30 min, and at 600 °C for 15 min, respectively. Mg–Al oxides, converted from NO<sub>3</sub>·Mg–Al LDHs with these conditions, were examined to treat HNO<sub>3</sub>. Table 2 shows the degree of NO<sub>3</sub><sup>-</sup> removal from HNO<sub>3</sub> solution by the Mg–Al oxides. All Mg–Al oxides were able to remove NO<sub>3</sub><sup>-</sup> from HNO<sub>3</sub> solution. As shown in Fig. 7, some NO<sub>3</sub><sup>-</sup> is remained in Mg–Al oxide obtained at 400 °C for 60 min. The remaining of NO<sub>3</sub><sup>-</sup> leads to the lowest degree of NO<sub>3</sub><sup>-</sup> removal for Mg–Al oxide obtained at 400 °C, although NO<sub>3</sub><sup>-</sup> removal for 500 °C was higher than that for 600 °C, although NO<sub>3</sub><sup>-</sup> was completely lost in Mg–Al oxides obtained at both temperatures. The high temperature probably promotes the crystallization of Mg–Al oxide for the conversion to MgO and MgAl<sub>2</sub>O<sub>4</sub>. This crystallization likely results in the decrease of NO<sub>3</sub><sup>-</sup> removal capability.

#### 4. Conclusions

The thermal decomposition of NO<sub>3</sub>·Mg–Al LDH occurred in the following four stages: evaporation of surface adsorbed water and interlayer water (stage 1), dehydroxylation of the brucite-like octahedral layers in NO<sub>3</sub>·Mg–Al LDH (stages 2 and 3), and elimination of NO<sub>3</sub><sup>--</sup> intercalated in the Mg–Al LDH interlayers to afford NO<sub>2</sub> (stage 4). The thermal properties of NO<sub>3</sub>·Mg–Al LDH were considered to be similar to those of Mg(OH)<sub>2</sub> and Mg(NO<sub>3</sub>)<sub>2</sub>. The temperature for H<sub>2</sub>O formation from the dehydroxylation of NO<sub>3</sub>·Mg–Al LDH was lower than that for NO<sub>2</sub> production. This observation was consistent with the thermodynamic consideration that the temperature for Mg(OH)<sub>2</sub> decomposition is lower than that for Mg(NO<sub>3</sub>)<sub>2</sub> decomposition. NO<sub>2</sub>, which was produced by the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH at 400–600 °C, reacted with H<sub>2</sub>O and

 $O_2$  to form HNO<sub>3</sub> and HNO<sub>2</sub>. The elimination of nitrogen oxides was found to increase with the decomposition time and temperature. Further, all the intercalated NO<sub>3</sub><sup>-</sup> was completely eliminated from NO<sub>3</sub>·Mg–Al LDH at 500 and 600 °C, confirming that Mg–Al oxide was produced upon the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH at 400–600 °C. The Mg–Al oxide was able to treat HNO<sub>3</sub> solution. To summarize, complete loss of nitrogen oxides of NO<sub>3</sub>·Mg–Al LDH and formation of Mg–Al oxide occurred in the thermal decomposition of NO<sub>3</sub>·Mg–Al LDH. On the basis of the present results, we concluded that cyclic usage of Mg–Al oxide for the treatment of HNO<sub>3</sub> is possible.

### References

- [1] F. Cavani, F. Trifiro, A. Vaccari, Catal. Today 11 (1991) 173.
- [2] S.P. Newman, W. Jones, New J. Chem. 22 (1998) 105.
- [3] A.D. Roy, Mol. Cryst. Liq. Cryst. 311 (1998) 173.
- [4] Y. You, G.F. Vance, H. Zhao, Appl. Clay Sci. 20 (2001) 13.
- [5] M.Z. Hussein, Z. Zainal, I. Yaziz, T.C. Beng, J. Environ. Sci. Health A 36 (2001) 565.
- [6] B. Dousova, V. Machovic, D. Kolousek, F. Kovanda, V. Dornicak, Water Air Soil Pollut. 149 (2003) 251.
- [7] L.P. Cardoso, J. Tronto, E.L. Crepaldi, J.B. Valim, Mol. Cryst. Liq. Cryst. 390 (2003) 49.
- [8] F. Li, Y. Wang, Q. Yang, D.G. Evans, C. Forano, X. Duan, J. Hazard. Mater. B125 (2005) 89.
- [9] S. Miyata, Clays Clay Miner. 31 (1983) 305.
- [10] L. Ingram, H.F.W. Taylor, Miner. Mag. 36 (1967) 465.
- [11] R. Allmann, Acta Cryst. B24 (1968) 972.
- [12] T. Kameda, F. Yabuuchi, T. Yoshioka, M. Uchida, A. Okuwaki, Water Res. 37 (2003) 1545.
- [13] R.L. Frost, A.W. Musumeci, M.O. Adebajo, W. Martens, J. Therm. Anal. Calorim. 89 (2007) 95.
- [14] S.J. Palmer, R.L. Frost, T. Nguyen, J. Therm. Anal. Calorim. 92 (2008) 879.
- [15] H.J. Spratt, S.J. Palmer, R.L. Frost, Thermochim. Acta 479 (2008) 1.
- [16] R.L. Frost, A. Soisnard, N. Voyer, S.J. Palmer, W.N. Martens, J. Raman Spectrosc. 40 (2009) 645.
- [17] S.J. Palmer, A. Soisnard, R.L. Frost, J. Colloid Interface Sci. 329 (2009) 404.
- [18] S.J. Palmer, H.J. Spratt, R.L. Frost, J. Therm. Anal. Calorim. 95 (2009) 123.
- [19] S.J. Palmer, R.L. Frost, T. Nguyen, Coord. Chem. Rev. 253 (2009) 250.
- [20] T. Kameda, T. Yoshioka, K. Watanabe, M. Uchida, A. Okuwaki, Appl. Clay Sci. 35 (2007) 173.
- [21] J. Madarasz, P.P. Varga, G. Pokol, J. Anal. Appl. Pyrol. 79 (2007) 475.
  [22] NIST Chemistry Webbook Standard Reference Database, No. 69, June 2005 Release. http://www.webbook.nist.gov/chemistry.
- [23] M. Binnewies, E. Milke, Wiley-VCH Verlag GmbH, Thermochemical Data of Elements and Compound, 2<sup>nd</sup> edn. Weinheim, 2002.
- [24] F.S. Chambers, T.K. Sherwood, Ind. Eng. Chem. 29 (1937) 1415.
- [25] M.S. Peters, C.P. Ross, J.E. Klein, AIChE J. 1 (1955) 105.